



Numerical Simulation of a Lead-Acid Battery Discharge Process using a Developed Framework on Graphic Processing Units

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Abstract

In the present work, a framework is developed for implementation of finite difference schemes on Graphic Processing Units (GPU). The framework is developed using the CUDA language and C++ template meta-programming techniques. The framework is also applicable for other numerical methods which can be represented similar to finite difference schemes such as finite volume methods on structured grids. The framework supports both linear and nonlinear finite difference stencils. Furthermore, the arithmetic operators and math functions are overloaded to ease the array-based computations on GPUs. The reduction algorithms are also efficiently included in the framework. The discharge process of a lead-acid battery cell is simulated using the facilities provided by the framework. The governing equations are unsteady and include two nonlinear diffusion equations for solid (electrode) and liquid (electrolyte) potentials and three transient equations for acid concentration, porosity and the state of charge. The equations are discretized using the finite volume method. The framework allows the user to develop the numerical solver with a few efforts. The numerical simulation results are reported for different relations for open circuit potential and the electrolyte diffusion coefficient.

Keywords:

CUDA,
Discharge Process,
Finite Difference
Method,
Finite Volume Method,
Graphics Processing
Units,
Lead-Acid Battery

Introduction

Using Graphics Processing Units (GPU) for numerical simulations has become popular in the scientific and engineering areas. Nowadays, high-end GPUs have several thousand computing cores that means they can simultaneously compute several thousand mathematical operations. The CUDA language is the most popular programming language for parallel processing using GPUs. However, due to the more complex structure of parallel programming and less debugging facilities, the development of a GPU numerical simulation code is a time-consuming task. In the present study, we developed a framework for using finite-difference schemes on GPUs. The framework includes several classes for defining array objects, mathematical expressions and finite difference schemes on the GPU device. The framework also includes

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several functions, which allows the user to easily implement loops for array computations. Another advantage of the present framework is that the reduction algorithms (i.e. computing the minimum, maximum or sum of the array elements) are efficiently implemented and the user can easily utilize them. It should be mentioned that the framework is also applicable for other numerical methods which can be represented similar to finite difference schemes such as finite volume methods on structured grids.

Due to the complexity of batteries, modeling and simulation are useful tools to optimize and analyze behavior and a better understanding of physical phenomena. Simulating the discharge process is important which enables researchers to predict the voltage drop of the battery cell as a function of time. The developed framework is utilized to simulate the discharge process of a lead-acid battery cell on a GPU. The model consists of unsteady nonlinear one-dimensional diffusion equations, which discretized using the finite volume method. The equations model the dynamic behavior of acid concentration, the porosity of the electrodes and the state of charge (SoC) of the cell. At each time step, an iterative algorithm solves the nonlinear system of equations. The results are validated by the previous works and presented for different empirical relations for the open circuit potential and the electrolyte diffusion coefficient.

Framework

To utilize the GPU cores in CUDA, one must write a GPU device function (or simply a kernel). This means even for a simple arithmetic operation; the user must write a kernel. In the present framework, using the C++ templates meta-programming techniques [1-3], which also supported by CUDA 7.0 and later versions, and overloading the arithmetic operators and math functions, the compiler automatically produces the required kernels (hidden from the user). For instance, in the following code, three arrays are defined and allocated on GPU memory with a size of 100 elements and then some operations are accomplished on:

```
#include <iostream>
#include <algorithm>
#include "exprNew.h"
#include "stencilExpr.h"
#include "cuarr.hpp"
#include "cuMakePatch.hpp"
#include "Stencil.hpp"
#include "Reduce.h"
#include <cmath>

using namespace std;

int main(int argc, char *argv[])
{
    int N = 100;

    cuarr<double> X;
    cuarr<double> Y;
    cuarr<double> T;

    X.Alloc(N);
    Y.Alloc(N);
    T.Alloc(N);

    X = 3.1415926;
    Y = 2 * X;
    T = sin(X + Y);

    return 0;
}
```

The files "exprNew.h", "stencilExpr.h", "cuarr.hpp", "cuMakePatch.hpp", "Stencil.hpp", and "Reduce.h" includes all the framework classes and functions definitions. In the above code, the three lines before "return 0" calculates some operations. The compiler produces and executes a kernel for each of the lines. As observed, the user writes a simple code and the compiler accomplishes the other time-consuming tasks.

Finite Difference Schemes

The framework provides two methods for defining finite difference operators. One is only suitable for linear schemes while the other method is suitable for both linear and nonlinear schemes.

A suitable way to express a linear stencil is to express it by the pairs of the (non-zero) coefficients and the corresponding distance from the base index. For instance, the central scheme for the first derivative can be expressed as:

$$\frac{1}{2h}f_{i+1} - \frac{1}{2h}f_{i-1} \rightarrow \left(\frac{1}{2h}, 1\right)\left(-\frac{1}{2h}, -1\right) \quad (1)$$

The framework allows the user to define and apply this scheme as:

```
Stencil1D<2> CentralSchemeStencil
(1, 1/(2*h), -1, -1/(2*h));

FiniteDifferenceOperator<2> CentralScheme;

CentralScheme.Set(CentralSchemeStencil);
T = CentralScheme(X);
```

However, this method is only applicable to linear schemes. The framework also allows for defining nonlinear schemes. For instance, the following relation,

$$A_E = \frac{\Gamma_i \Gamma_{i+1}}{\beta \Gamma_{i+1} + (1 - \beta) \Gamma_i} \times \frac{2}{d_{i+1} + d_i} \quad (2)$$

$$\beta = \frac{d_i}{d_{i+1} + d_i}$$

which appears in discretizing a diffusion equation using the finite volume method is defined (outside the main function) as:

```
struct AE :public SpecificStencil<AE>
{
    __device__ static double apply(int I,
        const cuarr<double>& G,
        const cuarr<double>& D)
    {
        return 2*G[I]*G[I+1] / (
            G[I+1] + D[I+1]/(D[I+1]+D[I])*(G[I]-G[I+1])) / (D[I]+D[I+1]);
    }
};
```

and then can be simply used as

```
T = AE::D(X, Y);
```

During the compilation, the compiler uses this single line and produces a kernel function and passes the input arrays (X and Y) to it. The produced kernel includes a call to the function `AE::apply`. The kernel loops this function over the entire elements of the array T.

Reduction Algorithms

Finding the minimum and maximum of an array and also calculating the sum of the array elements are common tasks in numerical simulations. These functions, which are called reduction algorithms, require special techniques to be efficiently computed in parallel processing. Although CUDA atomic functions are provided for these tasks, they do not utilize the parallel capability of the GPU device for accelerating the computations. In addition, the atomic functions are not defined for all data types. In the framework, without using atomic functions, the reduction algorithms are implemented by exploiting the parallel capability of the GPU device and the user just calls these functions as below

```
double diffMax = max(fabs(X-Y), N);
double diffMin = min(fabs(X-Y), N);
double sumT = sum(T, N);
```

Governing Equations

In this section, we present the equations govern the discharge process of a lead-acid battery cell. Fig. 1 shows a typical schematic of a lead-acid cell. The cell consists of the following regions: lead-grid collector at $x = 0$ which is at the center of the positive electrode; a positive electrode (PbO_2); an electrolyte reservoir; a porous separator; a negative electrode (Pb), and finally a lead-grid collector at $x = L$ located at the center of the negative electrode. The electrolyte reservoir is an ionic conductive medium, which transfers anions and cations between the two electrode matrices. The separator is a porous zone with two significant roles; firstly, it keeps cathode and anode apart as not to make a short circuit. Secondly, it is a porous zone allowing positive and negative ions to transfer easily. The two electrodes are made from a highly electronically conductive material with small pores filled by binary sulfuric acid, H_2SO_4 [4].

The model is a one-dimensional model of a battery cell discharge process. The details of the model can be found in [5,6]. The governing equations are as follows:

$$\frac{\partial}{\partial x} (\sigma^{\text{eff}} \frac{\partial \phi_s}{\partial x}) = Aj \quad (3)$$

$$\frac{\partial}{\partial x} (k^{\text{eff}} \frac{\partial \phi_l}{\partial x}) + \frac{\partial}{\partial x} (k_D^{\text{eff}} \frac{\ln c}{\partial x}) = -Aj \quad (4)$$

$$\frac{\partial \varepsilon c}{\partial t} = \frac{\partial}{\partial x} (D^{\text{eff}} \frac{\partial c}{\partial x}) + a_2 \frac{Aj}{2F} \quad (5)$$

$$\frac{\partial \varepsilon}{\partial t} = a_1 \frac{Aj}{2F} \quad (6)$$

$$\frac{\partial \text{SoC}}{\partial t} = \pm \frac{Aj}{Q_{\text{max}}} \quad \begin{cases} + & \text{PbO}_2 \text{ electrode} \\ - & \text{Pb electrode} \end{cases} \quad (7)$$

The field variables are given in Table 1. Eqs. 3 and 4 are of elliptic type which governs the conservation of charge in solid (the positive and negative electrodes) and electrolyte, respectively. Eqs. 5-7 give the time variation of the acid concentration c (multiplied by ε), the porosity ε and the state of charge (SoC), respectively. The different variables and constants, appeared in the equations, are as follows (in the cgs system of units):

$$\sigma^{\text{eff}} = \sigma(1 - \varepsilon)^{\text{ex}}, \quad k^{\text{eff}} = k\varepsilon^{\text{ex}}, \quad k_D^{\text{eff}} = k_D\varepsilon^{\text{ex}} \quad (8)$$

$$k = c \exp \left[1.1104 + (199.475 - 16097.781c)c + \frac{3916.95 - 99406c - \frac{712860}{T}}{T} \right] \quad (9)$$

$$k_D = \frac{RTk}{F} (2t_+^0 - 1), \quad F = 96485.33289, \quad R = 8.314 \quad t_+^0 = 0.72 \quad (10)$$

$$A = A_{\max} S_0 C^\xi, \quad A_{\max} = 100 \quad (11)$$

$$j = i_0 \left(\frac{c}{c_{\text{ref}}} \right)^\gamma \left[\exp \left(\frac{\alpha_a F}{RT} \eta \right) - \exp \left(\frac{-\alpha_c F}{RT} \eta \right) \right], \quad \alpha_a = \alpha_c = 0.5, \quad \gamma = 1.5 \quad (12)$$

$$\eta = \begin{cases} \phi_s - \phi_l - \Delta U_{\text{PbO}_2} & \text{PbO}_2 \text{ electrode} \\ \phi_s - \phi_l & \text{Pb electrode} \end{cases}$$

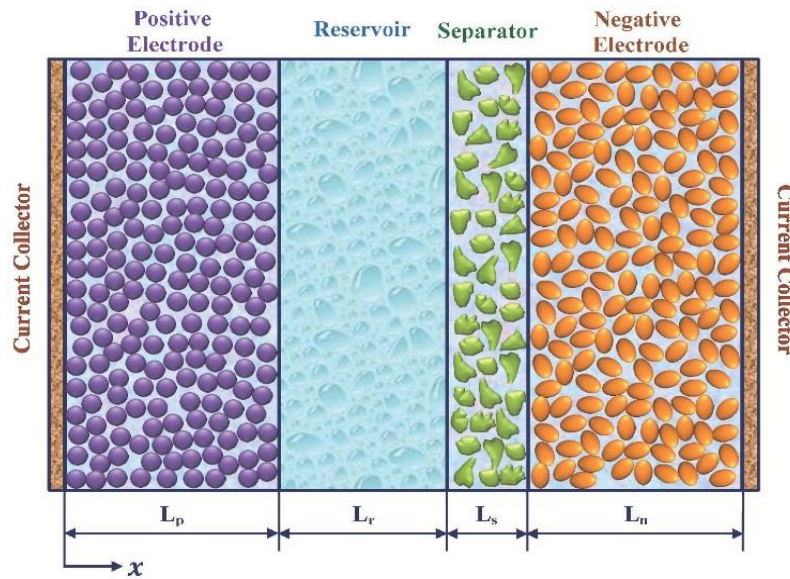


Fig. 1. Schematic of a lead-acid battery cell, with courtesy of Ref. [4].

The open circuit potential (ΔU_{PbO_2}) and the electrolyte diffusion coefficient (D) depend on acid concentration. However, it is a common practice to assume constant values for these variables, especially for ΔU_{PbO_2} [4-6]:

$$\Delta U_{\text{PbO}_2} = 2.095, \quad D = 3.02 \times 10^{-5} \quad (13)$$

here we also consider the following empirical relations [5,7]:

$$D = (1.75 + 260c) \times 10^{-5} \exp \left(\frac{2174}{298.15} - \frac{2174}{T} \right) \quad (14)$$

$$\Delta U_{\text{PbO}_2} = 0.0336 \log(m)^4 + 0.07377 \log(m)^3 + 0.06355 \log(m)^2 + 0.14751 \log(m) + 1.922 \quad (15)$$

$$m = 1.00322 \times 10^3 c + 3.55 \times 10^4 c^2 + 2.17 \times 10^6 c^3 + 2.06 \times 10^8 c^4$$

The state of the battery and initial conditions are given in Table 2. The boundary conditions are as follows:

$$\frac{\partial c}{\partial x} \Big|_{x=0,L} = 0, \quad \frac{\partial \phi_l}{\partial x} \Big|_{x=0,L}, \quad \phi_s(0) = V, \quad \phi_s(L) = 0 \quad (16)$$

The battery cell undergoes a discharge process at an applied current density of $I = 0.34 \text{ A cm}^{-2}$. The cell voltage (V) in the left boundary condition is not known and must be determined in order that the applied current density (I) equals the determined value (0.34 A cm^{-2}). The applied current density is computed by:

$$I = \int_{Pbo_2} A_j dx \quad (17)$$

Table 1. Field variables used in the governing equations of the battery

Property	Symbol
Solid potential	ϕ_s
Liquid potential	ϕ_e
Acid concentration	c
Porosity	ε
State of charge	SoC
Specific electroactive area	A
Transfer current density	j
Conductivity of solid	σ
Conductivity of liquid	k
Diffusion conductivity of liquid	k_D
Electrolyte diffusion coefficient	D
Temperature	T

Table 2. Initial conditions

Property	PbO ₂	Reservoir	Separator	Pb
c	0.0049	0.0049	0.0049	0.0049
ε	0.53	1.0	0.73	0.53
SoC	1.0	---	---	1.0
ex	1.5	1.0	3.53	1.5

The equations are discretized using the finite volume method. At each time step, a value is guessed for V and then the discretized form of Eqs. 3 and 4 are solved using the Newton iteration technique. The guessed value of V is updated by the Secant method until the applied current density converges to the desired value and then the solution marches to the next time step using Eqs. 5-7. The time-marching continues until V drops below a cut-off voltage. Here, the cut-off voltage is 1.5 V

Results and Discussion

All the field variables (Table 1) are defined as array objects. Also, most of the relations are implemented by the provided classes in the framework. For instance, the transfer current density (j) is implemented as follows:

```

struct TransferCurrentDensity : public MultiVarFun < TransferCurrentDensity >
{
    __device__ static double apply(double c, double eta, double T)
    {
        double res =
            i0*pow(c / c_ref, gamma)*
            (
                exp(alpha_a*cu_F*eta / (cu_R*T)) -
                exp(-alpha_c*cu_F*eta / (cu_R*T))
            );
        return res;
    }
};

```

A non-uniform grid is used for discretizing the geometry. The grid is clustered near the interface of the different regions. Eqs. 5-7 are integrated using the forward Euler method. Also, the discretized equations of the elliptic equations for the i -th volume can be written in the following general form [8]:

$$a_P \phi_i = a_W \phi_{i-1} + a_E \phi_{i+1} + S_u \quad (18)$$

$$a_P = a_W + a_E + S_P \quad (19)$$

$$a_E = \frac{\Gamma_e}{x_{i+1} - x_i} \quad a_W = \frac{\Gamma_w}{x_i - x_{i-1}}$$

where x_i is the position of the volume center and Γ is the diffusion coefficient (σ^{eff} or k^{eff}). The subscripts w and e indicate the left and right faces of the volume, respectively. The harmonic mean is used for approximating the diffusion coefficients (Γ) at the interface of two adjacent volumes:

$$\Gamma_e = \frac{\Gamma_i \Gamma_{i+1}}{\beta \Gamma_{i+1} - (1 - \beta) \Gamma_i} \quad (20)$$

$$\beta = \frac{x_e - x_i}{x_{i+1} - x_i}$$

which reduces the relation of a_E into scheme (2).

Fig. 2 shows the acid concentration at several times, using the empirical relations (Eqs. 14 and 15). The decrease of the acid concentration in the positive electrode is faster than that of the other regions. Fig. 3 shows the cell voltage (V) during the discharge process. The simulation results corresponding to relations (13) are also validated by those of Gu et al [5]. The figure shows using a constant value for the open circuit potential (ΔU_{PbO_2}) significantly affects the rate of the voltage drop. On the contrary, using a constant value for the electrolyte diffusion coefficient (D) has a slight effect on the rate of the voltage drop. Therefore, while assuming a constant value for the electrolyte diffusion coefficient is a good approximation, this is not the case for the open circuit potential.

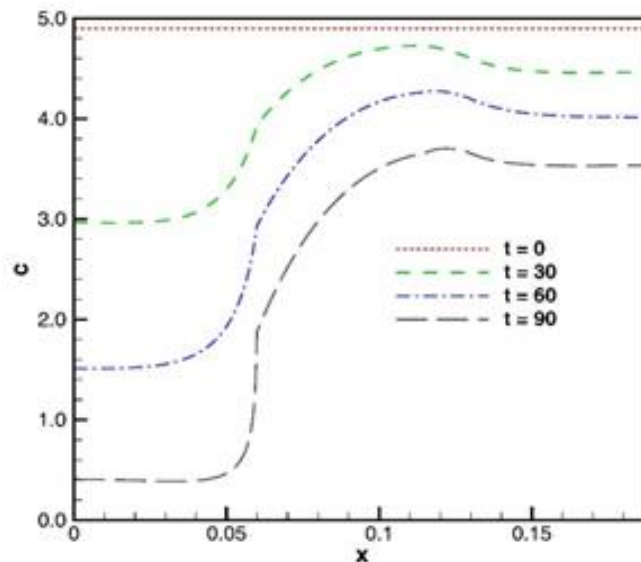


Fig. 2. Acid concentration during discharge.

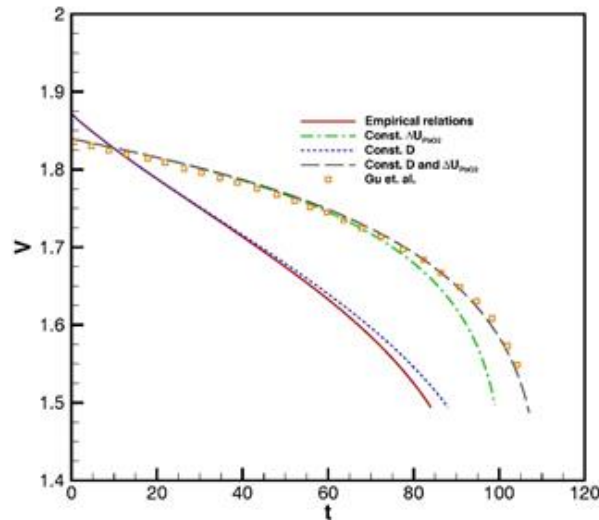


Fig. 3. Voltage of the cell during discharge

Conclusions

In the present work, the numerical simulation of a lead-acid battery cell was carried out using a GPU framework. The framework facilitated the GPU implementation of a finite difference (or structured finite volume) numerical simulation code using C++ meta-programming techniques. It was observed the arithmetic operators, math functions, linear and nonlinear schemes were used or defined without writing a GPU kernel. The simulations indicate while assuming a constant value for the electrolyte diffusion coefficient has a negligible effect on the rate of the voltage drop, assuming a constant value for the open circuit potential significantly affects this rate.

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