



New Correlations for Predicting Thermodynamic Properties of Hydrocarbons in the Ideal Gas State

Victor L. Malyshev , Elena F Moiseeva *

1. Ufa State Petroleum Technological University, Ufa, Russia. E-mail: p19105@usptu.ru
2. Ufa State Petroleum Technological University, Ufa, Russia. E-mail: p18729@usptu.ru

ARTICLE INFO	ABSTRACT
<p>Article History: Received: 10 April 2025 Revised: 10 July 2025 Accepted: 26 August 2025 Published: 26 August 2025</p> <p>Article type: Research</p> <p>Keywords: Enthalpy, Entropy, Heat Capacity, Ideal Gas State, Petroleum Fractions, Thermodynamic Correlation</p>	<p>A new empirical correlation is developed for the accurate prediction of isobaric heat capacity, enthalpy, and entropy of pure hydrocarbons and petroleum fractions in the ideal gas state, with a particular emphasis on the low-temperature region (200–300 K). Unlike traditional models such as Kesler-Lee, Huang, and Kuznetsov, which are often limited in accuracy or applicability at low temperatures or for heavy hydrocarbons, the proposed correlation integrates a fourth-degree polynomial approach and molecular weight dependence to extend predictive capabilities across a broad range of components—from butane to heavy fractions exceeding 570 g/mol. Validation against 340 experimental data points for heat capacity and 112 data points for enthalpy and entropy reveals a significant reduction in AARE and MARE values, achieving errors of 0.90% and 2.10%, respectively. While the correlation provides excellent results for normal alkanes, its applicability to cycloalkanes and aromatic hydrocarbons is limited and may require further refinement. The proposed model holds strong potential for implementation in thermodynamic simulators for oil, gas, and condensate production and processing, especially under surface conditions where precise thermophysical data at subambient temperatures are critical.</p>

Introduction

The integration of new technologies in the oil and gas industry imposes increasing demands on engineers' knowledge, particularly in understanding the behavior of complex systems. For efficient design of chemical, petrochemical, and biochemical processes in a wide range of pressures and temperatures, accurate data on the thermodynamic properties of pure hydrocarbons and petroleum fractions are required. Phase behavior and thermal properties, which are essential for designing technological processes, are typically not determined for all compounds and must be estimated using thermodynamic models.

In petroleum engineering, models based on equations of state are widely used to calculate thermodynamic properties, as they enable the prediction of phase state and thermodynamic properties over a wide range of pressures and temperatures. Most of these models use the ideal gas state as a reference state for thermodynamic calculations. Thus, for accurate simulations of technological processes, it is necessary to know the properties of fluid in the ideal gas state over a wide range of thermobaric conditions. According to thermodynamic relations, most functions of the ideal gas state can be derived from the heat capacity.

* Corresponding Author: E.F. Moiseeva (E-mail address: p18729@usptu.ru)



One of the earliest correlations for the ideal gas heat capacity for hydrocarbons was proposed in [1, 2] and was described by a polynomial function of temperature. Aly and Lee [3] introduced expressions for the ideal gas heat capacity derived theoretically from thermodynamic relations. This method provides accurate predictions of heat capacity, enthalpy and entropy for many compounds over a temperature range from 300 K to 1500 K. Coniglio et al. [4] developed approaches based on statistical mechanics that allow the calculation of the ideal gas heat capacity below 300 K. However, authors considered only a limited number of compounds, and their approaches cannot be applied to complex mixtures such as crude oil.

Correlations for thermodynamic properties of various gases in the ideal gas state, based on the molecular structure of fluid compounds, can be found in [5-8]. However, due to the discrete nature of the data set, there are some definite limitations to the use of the correlations they propose.

Heavy hydrocarbons have a large number of isomers, which requires an increased number of initial parameters for accurate estimation of their heat capacity. Attempts have been made to utilize critical parameters (pressure, temperature, and volume), the Watson characterization factor, the acentric factor, molecular weight, and other parameters to calculate thermodynamic properties. Each of the parameters can be independently estimated using the graphical methods of Watson and Nelson [9], API [10], and one of the analytical correlations of Cavett [11], Kesler-Lee [12], Lee-Kesler [13], Riazi-Daubert [14, 15], Riazi-Sahhaf [16], Twu [17], Pedersen [18-21], and Korsten [22], which are presented in detail in the Riazi monograph [23].

Currently, in petroleum engineering, the Kesler-Lee correlation [12] is the most widely used for calculating the heat capacity of petroleum fractions. It is implemented in modern software for PVT simulations such as PVTsim Nova by Calsep, Multiflash by KBC, and Aspen HYSYS.

The correlations described above provide high accuracy in most cases; however, with the advancement of high-precision chromatography and more accurate computational methods, further modifications remain relevant. A universal correlation for determining the ideal gas heat capacities of large and complex molecules is presented in [24]. In the work [25], the authors propose a correlation for calculating the heat capacity and enthalpy of an ideal gas. It demonstrates significantly improved accuracy compared to the Kesler-Lee method, thereby opening new possibilities for more precise thermodynamic modeling of hydrocarbon systems. Meanwhile, for pure hydrocarbons, Kuznetsov proposed a simple correlation for heat capacity calculation based solely on the carbon number [26, 27]. Despite its simplicity, this model is only applicable within the temperature range from 298.15 to 1500 K.

In this work, we propose a new correlation for calculating the heat capacity, enthalpy, and entropy of petroleum fractions, extending its applicability to low temperatures down to 200 K. The obtained results are compared with established models from other authors.

Mathematical Model

Heat Capacity

Numerous correlations have been developed for calculating the heat capacity c_p^{id} of hydrocarbons in the ideal gas state for various conditions and parameters. In this section, we'll consider the most common ones.

Kesler & Lee, 1976

Kesler & Lee correlation [12] is “classical” for most PVT software. They proposed two different models for calculating c_p^{id} . The first correlation is presented for fractions C_{7+} [23]:

$$c_p^{id} = 4.1868 M_w [C_0 + C_1 T + C_2 T^2] \quad (1)$$

$$\begin{aligned} C_0 &= -0.32646 + 0.02678 K_W - C_{F0}(0.084773 - 0.080809 SG), \\ C_1 &= [-2.5006 + 2.182 K_W - 0.06845 K_W^2 + C_{F0}(3.9191 - 3.7487 SG)] \times 10^{-4}, \\ C_2 &= [-4.9874 - C_{F0}(2.54823 - 2.28171 SG)] \times 10^{-7}, \\ C_{F0} &= \left[100 \left(\frac{12.8}{K_W} - 1 \right) \left(\frac{10}{K_W} - 1 \right) \right]^2, \\ K_W &= \frac{T_b^{1/3}}{SG}, \end{aligned}$$

where SG is specific gravity, which is approximately equal to the liquid density, T_b is the normal boiling temperature in K; K_W - Watson characterization factor; M_w is molecular weight in g/mol; c_p^{id} - heat capacity in the ideal gas state in J/mol·K; T is temperature in K.

The second Kesler and Lee (Lee-Kesler 2) [24] correlation for direct calculation of c_p^{id} of petroleum fractions, in terms of the Watson factor and acentric factor:

$$c_p^{id} = M_w [A_0 + A_1 T + A_2 T^2 - C_F (B_0 + B_1 T + B_2 T^2)] \quad (2)$$

$$\begin{aligned} A_0 &= -1.41779 + 0.11828 K_W, \\ A_1 &= -(6.99724 - 8.69326 K_W + 0.27715 K_W^2) \times 10^{-4}, \\ A_2 &= -2.2582 \times 10^{-6}, \\ B_0 &= 1.09223 - 2.48245 \omega, \\ B_1 &= -(3.434 - 7.14 \omega) \times 10^{-3}, \\ B_2 &= -(7.2661 - 9.2561 \omega) \times 10^{-7}, \\ C_F &= \left[\frac{(12.8 - K_W)(10 - K_W)}{10 \omega} \right]^2 \end{aligned}$$

Acentric factor ω is defined from the following correlations [13].

For $T_{br} \leq 0.8$

$$\omega = \frac{-\ln \frac{P_c}{1.01325} - 5.92714 + \frac{6.09648}{T_{br}} + 1.28862 \ln(T_{br}) - 0.169347 T_{br}^6}{15.2518 - \frac{15.6875}{T_{br}} - 13.4721 \ln(T_{br}) + 0.46577 T_{br}^6}$$

For $T_{br} > 0.8$

$$\omega = -7.904 + 0.1352 K_W - 0.007465 K_W^2 + 8.359 T_{br} + \frac{1.408 - 0.01063 K_W}{T_{br}}$$

where $T_{br} = T_b/T_c$, P_c , T_c are the critical pressure (bar) and temperature (K) of the fraction, respectively.

Huang, 2019

One more correlation is presented in [25]. Based on the experimental data for pure components from C_7 to C_{40} in the temperature range from 200 to 1000 K, the authors derived the following correlation using regression analysis:

$$c_p^{id} = M_w \left[\begin{aligned} &0.0240296 + 0.0062421 T - 2.60151 \times 10^{-6} T^2 + \\ &+ C_F (0.0022514 - 1.15054 \times 10^{-5} T + 2.39542 \times 10^{-8} T^2) \end{aligned} \right] \quad (3)$$

The designations and dimensions are the same as those presented earlier.

Kuznetsov, 2021

In 2021, Kuznetsov N.M. and Frolov S.M. proposed a simple analytical correlation for heat capacity and enthalpy [26]. They considered the heat capacity and enthalpy of saturated hydrocarbons in the ideal gas state, which depend on temperature and the number of carbon atoms in a molecule.

Using the experimental data for pure alkanes from C₅ to C₂₀, they derived the equation:

$$c_p^{id} = c_{p,5}(T) + g(T)(n - 5) \quad (4)$$

$$c_{p,5}(T) = -4.0338 + 48.8733\tau - 2.5967\tau^2 + 0.0536\tau^3,$$

$$g(T) = -0.6528 + 9.3799\tau - 0.5309\tau^2 + 0.0116\tau^3,$$

where τ is the dimensionless temperature in 100 K ($\tau = T/100$).

New correlation

As noted in [28], most correlations are derived for the temperature range from 300 K to 1500 K, and, therefore, cannot be reliably extrapolated to lower temperatures. Considering that the average boiling point of the C₈₀ fraction is about 950 K [29], we will look for correlations in the range from 200 to 1000 K to calculate properties of the fluid in the ideal gas state.

According to the experimental data from [25] given in Table 1, we'll plot the temperature dependence of c_p^{id} for n-alkanes C₇, C₁₅, C₂₀, C₃₀, and C₄₀ (Fig. 1).

Table 1. Data used for fitting and testing the isobaric heat capacity of petroleum fractions in the ideal gas state [25]

C _n	c_p^{id} (J/mol·K)									
	T (K)									
	200	298.15	300	400	500	600	700	800	900	1000
C ₇	127.65	165.18	165.98	210.66	252.09	287.44	317.15	342.25	363.59	381.58
C ₈	144.77	187.78	188.7	239.74	286.81	326.77	360.24	388.28	411.71	431.37
C ₉	161.92	210.41	211.42	268.77	321.54	366.1	403.34	433.88	459.82	481.58
C ₁₀	179.08	233.05	234.18	297.98	356.43	405.85	446.43	479.9	508.36	531.79
C ₁₁	196.23	255.68	256.94	327.15	391.33	445.18	489.53	525.93	556.89	581.99
C ₁₂	213.38	278.32	279.7	356.31	426.35	484.93	532.62	571.95	605.01	632.2
C ₁₃	230.54	300.96	302.46	385.47	461.08	524.67	576.14	618.4	653.54	682.41
C ₁₄	247.69	325.26	325.22	414.63	496.22	564	619.23	664.42	702.08	732.62
C ₁₅	264.85	346.23	347.98	443.92	530.95	603.33	662.33	710.44	750.61	782.83
C ₁₆	282	368.86	370.74	472.79	565.68	643.08	705.42	756.47	798.73	833.03
C ₁₇	299.16	391.5	393.51	502.08	600.82	682.83	748.52	802.49	847.26	883.24
C ₁₈	316.31	414.13	416.27	531.37	635.55	722.16	792.03	848.93	895.79	933.45
C ₁₉	333.46	436.81	438.9	560.66	670.28	761.49	835.13	894.96	943.91	983.66
C ₂₀	350.62	459.4	461.91	589.53	705.42	801.24	878.22	940.98	992.44	1033.87
C ₂₁	367.77	482.04	484.67	618.69	740.32	840.77	921.4	987.09	1040.85	1084.07
C ₂₂	384.93	504.67	507.44	647.85	775.21	880.31	964.58	1033.2	1089.26	1134.28
C ₂₃	402.08	527.31	530.2	677.01	810.11	919.85	1007.76	1079.3	1137.67	1184.49
C ₂₄	419.24	549.94	552.96	706.18	845	959.39	1050.94	1125.41	1186.08	1234.7
C ₂₅	436.39	572.58	575.72	735.34	879.9	998.93	1094.12	1171.52	1234.49	1284.91
C ₂₆	453.55	595.22	598.48	764.5	914.79	1038.47	1137.29	1217.63	1282.9	1335.11
C ₂₇	470.7	617.85	621.24	793.66	949.68	1078.01	1180.47	1263.74	1331.31	1385.32
C ₂₈	487.85	640.49	644	822.83	984.58	1117.55	1223.65	1309.84	1379.72	1435.53
C ₂₉	505.01	663.12	666.76	851.99	1019.47	1157.09	1266.83	1355.95	1428.12	1485.74
C ₃₀	522.16	685.76	689.52	881.15	1054.37	1196.62	1310.01	1402.06	1476.53	1535.95
C ₃₁	539.32	708.39	712.28	910.31	1089.26	1236.16	1353.19	1448.17	1524.94	1586.15
C ₃₂	556.47	731.03	735.05	939.48	1124.16	1275.7	1396.37	1494.27	1573.35	1636.36
C ₃₃	573.63	753.66	757.81	968.64	1159.05	1315.24	1439.55	1540.38	1621.76	1686.57
C ₃₄	590.78	776.3	780.57	997.8	1193.95	1354.78	1482.73	1586.49	1670.17	1736.78
C ₃₅	607.94	798.93	803.33	1026.96	1228.84	1394.32	1525.9	1632.6	1718.58	1786.99
C ₃₆	625.09	821.57	826.09	1056.13	1263.74	1433.86	1569.08	1678.7	1766.99	1837.19
C ₃₇	642.24	844.21	848.85	1085.29	1298.63	1473.4	1612.26	1724.81	1815.4	1887.4
C ₃₈	659.4	866.84	871.61	1114.45	1333.52	1512.93	1655.44	1770.92	1863.8	1937.61
C ₃₉	676.55	889.48	894.37	1143.61	1368.42	1552.47	1698.62	1817.03	1912.21	1987.82
C ₄₀	693.71	912.11	917.13	1172.78	1403.31	1592.01	1741.8	1863.14	1960.62	2038.03

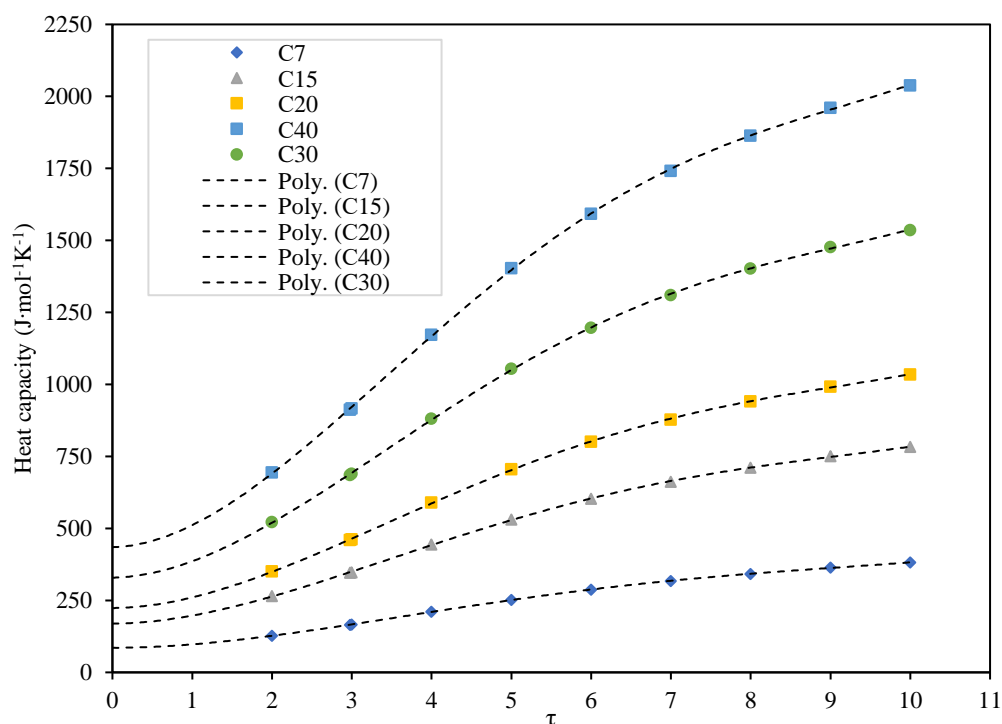


Fig. 1. Fitting the experimental data for c_p^{id} of n-alkanes C7, C15, C20, C30, and C40

Approximating the data from Table 1 with a third-degree polynomial fails to accurately describe the heat capacity of hydrocarbons in both low- and high-temperature regions simultaneously. However, switching to a fourth-degree polynomial enables the reproduction of the inflection point observed in the 200–400 K range (Fig. 1). Numerical calculation of the heat capacity derivative for n-heptane (Fig. 2), using data from the NIST database, confirms this inflection point within the specified range. Consequently, a fourth-order polynomial was used to approximate thermodynamic properties in this study. For convenience, the reduced temperature parameter $\tau = T/100$ was employed.

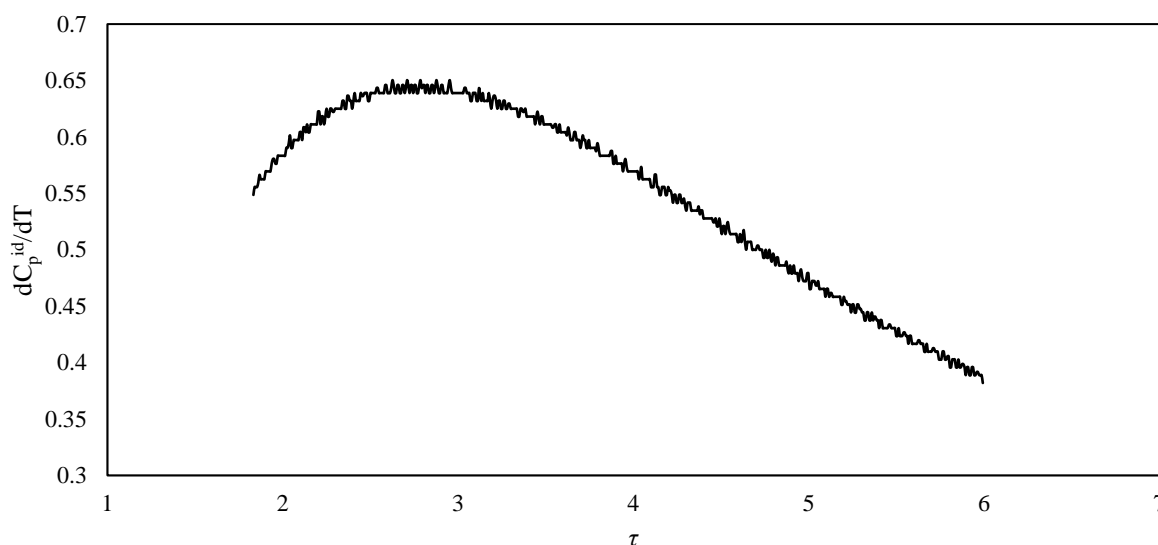


Fig. 2. Dependence of c_p^{id}/dT on τ for n-heptane

According to the regression analysis for hydrocarbons C_7 and C_8 , the polynomials were found:

$$\begin{aligned} c_{p,n=7}^{id}(T) &= 0.07\tau^4 - 1.79\tau^3 + 13.90\tau^2 - 0.37\tau + 85.43, \\ c_{p,n=8}^{id}(T) &= 0.08\tau^4 - 2.04\tau^3 + 15.75\tau^2 + 0.30\tau + 95.59. \end{aligned}$$

Because alkanes C_n and C_{n+1} differ from each other by the radical CH_2 [26], the increase in the carbon number by one leads to a linear dependence of the heat capacity on the number of carbon atoms n at constant temperature. In such a case, the linearization of the heat capacity can be written as:

$$c_{p,n}^{id}(T) = c_{p,n=7}^{id}(T) + f(T)(n - 7) \quad (5)$$

We define the function $f(T)$ based on the approximation of n -hexane and n -octane.

$$f(T) = c_{p,n=8}^{id}(T) - c_{p,n=7}^{id}(T) = 0.01\tau^4 - 0.25\tau^3 + 1.85\tau^2 + 0.66\tau + 10.16.$$

In most cases, technological processes involve hydrocarbon mixtures where the C_{7+} component composition is defined not by pure hydrocarbons but by petroleum fractions. These fractions are typically characterized in most software packages using two parameters: molecular weight (M_w) and liquid-phase specific gravity (SG). As shown in the Katz-Firoozabadi table [30], the relationship between a fraction molecular weight and its carbon number is nearly linear (Fig. 3) and can be approximated by the expression:

$$M_w = 14.027n + 2.016 \quad (6)$$

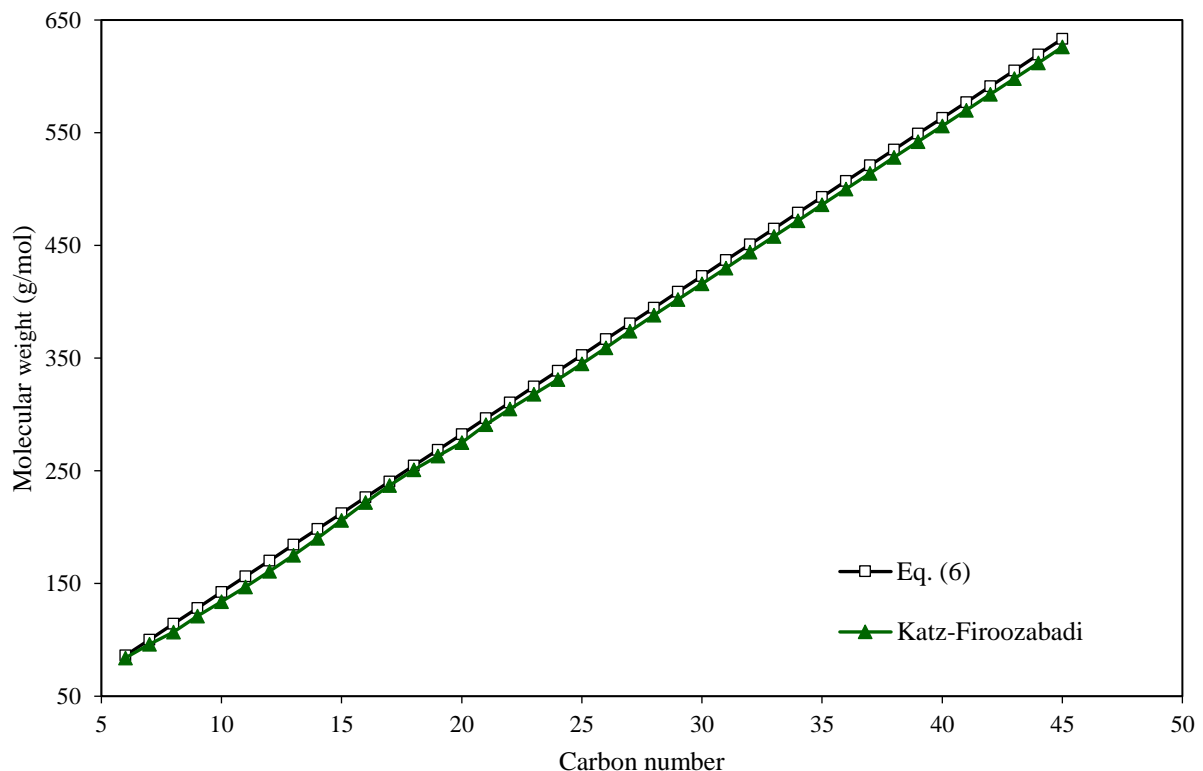


Fig. 3. Molecular weight of fraction C_n as a function of carbon number for pure alkanes and petroleum fractions

Combining Eqs. 5 & 6, we obtain:

$$\begin{aligned}
 c_{p,n}^{id}(T) &= c_{p,0}^{id}(T) + \alpha(T)M_w, \\
 c_{p,0}^{id}(T) &= -0.0002\tau^4 - 0.0017\tau^3 + 0.6835\tau^2 - 5.1153\tau + 12.8826, \\
 \alpha(T) &= 0.0007\tau^4 - 0.0179\tau^3 + 0.1319\tau^2 + 0.0474\tau + 0.724.
 \end{aligned} \tag{7}$$

The extension of the Katz-Firoozabadi table to heavy components of C_{80} [29] reveals a nonlinear relationship between molecular weight and the carbon number of the fraction. This dependence can be approximated using a second-order or higher polynomial. The functional relationship $M_w = M_w(n)$ may also serve as a modification of Eq. 6.

Enthalpy

According to thermodynamic relations, the enthalpy for an ideal gas state can be determined from the heat capacity as follows:

$$H_n^{id}(T) = \int_{T_1}^T c_{p,n}^{id}(T) dT + H_n^{id}(T_1).$$

Using Eq. 7, enthalpy can be expressed as:

$$H_n^{id}(T) = \int_{T_1}^T (c_{p,0}^{id}(T) + \alpha(T)M_w) dT + H_n^{id}(T_1) \tag{8}$$

We choose $T_1 = 300$ K as a reference point. The integration constant is determined from linearization of experimental data from [31] (Table 2) through the values of n-heptane $H_7^{id}(T_1) = 32171$ J/mol and n-eicosane $H_{20}^{id}(T_1) = 86734$ J/mol:

$$H_n^{id}(T_1) = H_7^{id}(T_1) + (n - 7) \frac{H_{20}^{id}(T_1) - H_7^{id}(T_1)}{13}.$$

Given the expression 6, the integration constant can be defined in terms of molecular weight:

$$H_n^{id}(T_1) = 299.22M_w + 2187.23. \tag{9}$$

After integration of the fourth-degree polynomials (7), the final expression for enthalpy calculation will be as follows:

$$\begin{aligned}
 H_n^{id}(T) &= H_0^{id}(T) + \beta(T)M_w, \\
 H_0^{id}(T) &= -0.004\tau^5 - 0.0425\tau^4 + 22.783\tau^3 - 255.765\tau^2 + 1288.26\tau + 13.6, \\
 \beta(T) &= 0.014\tau^5 - 0.4475\tau^4 + 4.3967\tau^3 + 2.37\tau^2 + 72.4\tau - 25.17, \\
 \tau &= T/100.
 \end{aligned} \tag{10}$$

Table 2. Data used for fitting and testing the enthalpy of petroleum fractions in the ideal gas state [31]

C _n	H _n ^{id} (J/mol)							
	T (K)							
	300.0	400.0	500.0	600.0	700.0	800.0	900.0	1000.0
C ₃	14836.5	23246.3	33639.4	45731.1	59371.0	74307.8	90374.4	107403.3
C ₄	19618.8	30710.6	44329.5	60149.2	77906.1	97336.6	118202.2	140331.4
C ₅	23773.5	37455.2	54266.5	73755.6	95596.0	119528.5	145163.9	172339.0
C ₆	27978.4	44266.7	64266.2	87412.1	113373.8	141753.9	172200.9	204388.4
C ₇	32170.8	51061.5	74245.1	101068.7	131122.4	164012.8	199237.9	236479.7
C ₈	36363.1	57856.4	84223.9	114725.3	148870.9	186238.2	226274.9	268529.1
C ₉	40568.1	64667.9	94223.7	128381.9	166619.4	208497.1	253274.3	300620.4
C ₁₀	44752.1	71253.5	104202.5	142038.4	184397.2	230722.5	280311.3	332669.8
C ₁₁	48965.4	78257.5	114202.3	155695.0	202145.8	252947.9	307310.6	364719.3
C ₁₂	53157.7	85069.1	124181.1	169351.6	219894.3	275206.8	334347.6	396810.6
C ₁₃	57350.1	91863.9	134160.0	182983.1	237642.8	297423.8	361384.6	428860.0
C ₁₄	61555.0	98658.7	144159.7	196639.6	255391.4	319657.6	388384.0	460909.4
C ₁₅	65747.4	105453.5	154138.6	210296.2	273169.2	341883.0	415421.0	492958.9
C ₁₆	69952.3	112265.1	164138.3	223952.8	290917.7	364141.9	442420.3	525050.2
C ₁₇	74144.7	119059.9	174117.2	237609.4	308666.2	386367.3	469457.4	557099.6
C ₁₈	78337.0	125854.7	184096.0	251265.9	326414.8	408592.7	496494.4	589149.0
C ₁₉	82542.0	132666.3	194095.8	264922.5	344163.3	430851.6	523493.7	621240.3
C ₂₀	86734.3	139461.1	204062.0	278579.1	361941.1	453077.0	550530.7	653289.8

Entropy

Entropy for a fluid in the ideal gas state can be obtained by integration of $c_{p,n}^{id}/T$

$$S_n^{id}(T) = \int_{T_1}^T \frac{c_{p,n}^{id}(T)}{T} dT + S_n^{id}(T_1).$$

The calculation procedure, similar to those for enthalpy, can be applied to entropy. Using the experimental data presented in Table 3 and choosing as reference points the entropy values of *n*-heptane $S_7^{id}(T_1) = 429$ J/mol·K and *n*-eicosane $S_{20}^{id}(T_1) = 937$ J/mol·K formula for entropy calculation is as follows:

$$S_n^{id}(T) = S_0^{id}(T) + \gamma(T)M_w, \quad (11)$$

$$S_0^{id}(T) = -0.00005\tau^4 - 0.000566\tau^3 + 0.34175\tau^2 - 5.1153\tau + 12.8826 \ln(\tau) + 147.7365,$$

$$\gamma(T) = 0.000175\tau^4 - 0.00596\tau^3 + 0.06595\tau^2 + 0.0474\tau + 0.724 \ln(\tau) + 1.4028.$$

Table 3. Data used for fitting and testing the entropy of petroleum fractions in the ideal gas state [31]

C _n	<i>S_n^{id}</i> (J/mol·K)							
	<i>T</i> (K)							
	300.00	400.00	500.00	600.00	700.00	800.00	900.00	1000.00
C ₃	270.37	294.43	317.52	339.53	360.54	380.49	399.45	417.44
C ₄	310.66	342.71	373.21	402.12	429.53	455.51	480.07	503.38
C ₅	349.74	388.90	426.27	461.66	495.30	527.27	557.39	586.01
C ₆	389.36	435.97	480.45	522.50	562.50	600.36	636.18	670.11
C ₇	428.86	482.92	534.46	583.21	629.48	673.41	714.79	754.04
C ₈	467.94	529.44	588.10	643.50	696.09	746.01	792.95	837.55
C ₉	507.06	576.01	641.70	703.79	762.70	818.60	871.19	921.07
C ₁₀	546.14	622.54	695.34	764.08	829.27	891.15	949.43	1004.62
C ₁₁	585.22	669.11	748.98	824.37	895.88	963.74	1027.63	1088.13
C ₁₂	624.34	715.63	802.57	884.66	962.49	1036.33	1105.83	1171.65
C ₁₃	663.42	762.16	856.21	944.91	1029.10	1108.93	1184.03	1255.16
C ₁₄	702.49	808.73	909.85	1005.21	1095.71	1181.52	1262.23	1338.67
C ₁₅	741.57	855.25	963.49	1065.50	1162.27	1254.07	1340.47	1422.23
C ₁₆	780.69	901.82	1017.09	1125.79	1228.88	1326.66	1418.67	1505.74
C ₁₇	819.77	948.35	1070.73	1185.87	1295.53	1399.26	1496.87	1589.25
C ₁₈	858.85	994.87	1124.37	1246.37	1362.06	1471.85	1575.07	1672.76
C ₁₉	897.97	1041.44	1177.96	1306.66	1428.71	1544.44	1653.27	1756.28
C ₂₀	937.05	1087.97	1231.60	1366.95	1495.28	1616.99	1731.51	1839.83

Results and Discussions

Based on 340 experimental values of c_p^{id} for pure alkanes from C₇ to C₄₀, a comparison of different methods to predict the heat capacity in the ideal gas state has been made. For enthalpy and entropy estimation, data from 112 experimental points were used (Tables 1-3) [31]. The accuracy of various correlations was evaluated using stochastic parameters, including AARE, MARE, MSE, RMSE, SD, and R² [32].

$$AARE = \frac{1}{N} \sum_{i=1}^N \left| \frac{c_{p,i}^{id,cal} - c_{p,i}^{id,exp}}{c_{p,i}^{id,exp}} \right| \times 100\%,$$

$$MARE = \max_i \left\{ \left| \frac{c_{p,i}^{id,cal} - c_{p,i}^{id,exp}}{c_{p,i}^{id,exp}} \right| \times 100\% \right\},$$

$$MSE = \frac{1}{N} \sum_{i=1}^N (c_{p,i}^{id,cal} - c_{p,i}^{id,exp})^2,$$

$$RMSE = \sqrt{\frac{1}{N} \sum_{i=1}^N (c_{p,i}^{id,cal} - c_{p,i}^{id,exp})^2},$$

$$SD = \sqrt{\frac{1}{N-1} \sum_{i=1}^N \left(c_{p,i}^{id,cal} - \text{average} \left(c_{p,i}^{id,exp} \right) \right)^2},$$
$$R^2 = 1 - \frac{\sum_{i=1}^N \left(c_{p,i}^{id,cal} - c_{p,i}^{id,exp} \right)^2}{\sum_{i=1}^N \left(c_{p,i}^{id,cal} - \text{average} \left(c_{p,i}^{id,exp} \right) \right)^2},$$

The results of heat capacity calculation using different methods are presented in [Tables 4-5](#) and [Figs. 4-5](#) (C_n will refer to n-alkanes with the formula C_nH_{2n+2}).



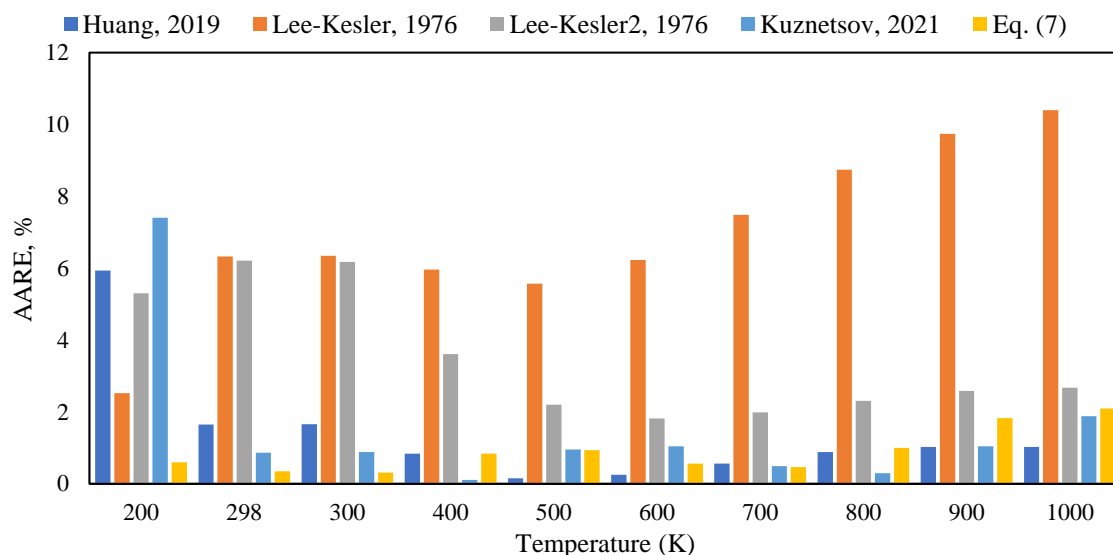
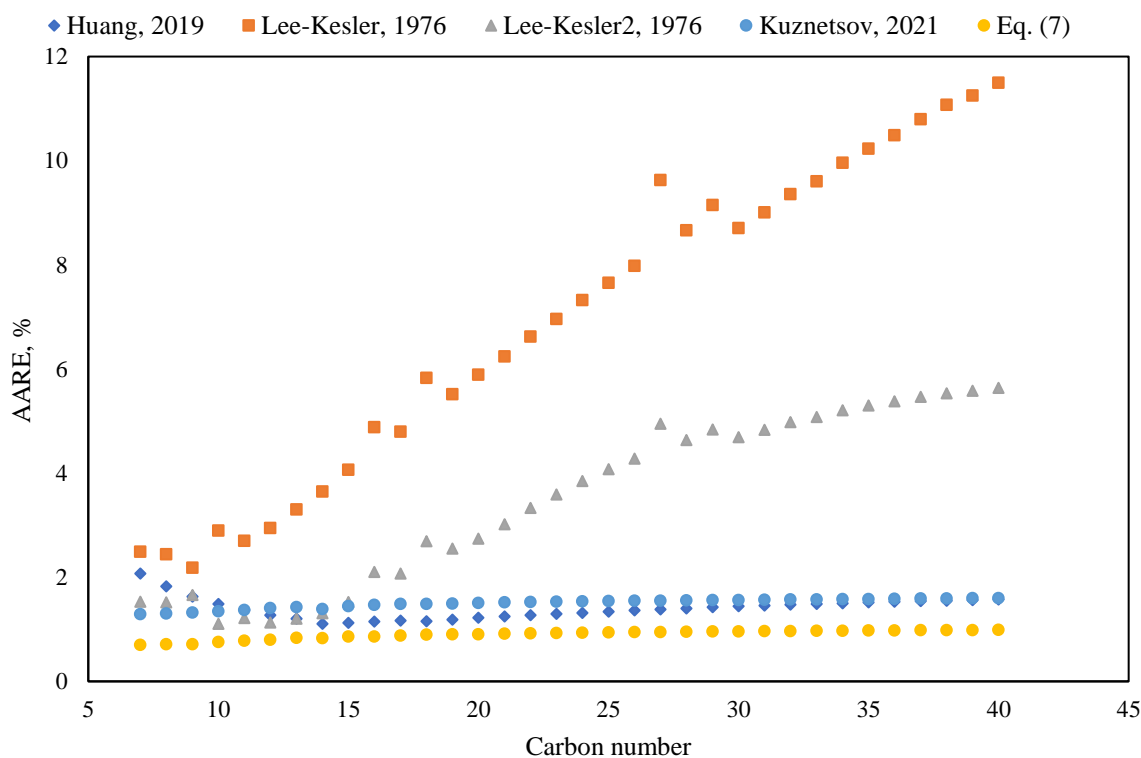
Table 4. Comparison of different correlations for heat capacity in the ideal gas state calculation in the temperature range 200-1000 K

C _n	NPTS	AARE, %					MARE, %				
		Huang, 2019	Lee-Kesler, 1976	Lee-Kesler2, 1976	Kuznetsov, 2021	Eq. 7	Huang, 2019	Lee-Kesler, 1976	Lee-Kesler2, 1976	Kuznetsov, 2021	Eq. 7
C ₇	10	2.07	2.48	1.53	1.29	0.70	8.28	6.97	6.30	9.20	1.49
C ₈	10	1.82	2.44	1.52	1.30	0.71	7.81	7.09	6.45	8.83	1.52
C ₉	10	1.62	2.18	1.66	1.32	0.71	7.45	7.72	7.05	8.56	1.63
C ₁₀	10	1.49	2.90	1.10	1.35	0.75	7.16	6.37	5.71	8.34	1.71
C ₁₁	10	1.37	2.69	1.22	1.37	0.78	6.93	6.77	6.12	8.16	1.79
C ₁₂	10	1.27	2.94	1.13	1.40	0.80	6.73	6.32	5.67	8.01	1.85
C ₁₃	10	1.20	3.30	1.20	1.42	0.83	6.56	6.47	4.99	7.88	1.90
C ₁₄	10	1.10	3.64	1.31	1.39	0.83	6.42	7.08	4.26	7.77	1.95
C ₁₅	10	1.12	4.06	1.52	1.44	0.86	6.29	7.62	3.60	7.68	1.98
C ₁₆	10	1.15	4.88	2.10	1.47	0.86	6.18	8.60	3.63	7.59	2.02
C ₁₇	10	1.16	4.79	2.07	1.48	0.88	6.08	8.64	3.51	7.52	2.05
C ₁₈	10	1.15	5.83	2.69	1.48	0.90	5.99	9.76	4.94	7.45	2.08
C ₁₉	10	1.18	5.51	2.55	1.49	0.90	5.91	9.54	4.50	7.39	2.10
C ₂₀	10	1.22	5.89	2.74	1.51	0.90	5.84	9.98	5.00	7.34	2.12
C ₂₁	10	1.25	6.24	3.02	1.51	0.91	5.78	10.38	5.47	7.29	2.14
C ₂₂	10	1.27	6.62	3.33	1.52	0.92	5.72	10.79	5.97	7.24	2.16
C ₂₃	10	1.30	6.95	3.59	1.53	0.93	5.66	11.14	6.41	7.20	2.18
C ₂₄	10	1.32	7.32	3.85	1.53	0.93	5.62	11.49	6.88	7.16	2.19
C ₂₅	10	1.34	7.65	4.07	1.54	0.94	5.57	11.81	7.31	7.13	2.21
C ₂₆	10	1.36	7.98	4.27	1.55	0.94	5.53	12.10	7.72	7.10	2.22
C ₂₇	10	1.38	9.63	4.94	1.55	0.95	5.49	13.21	9.57	7.07	2.23
C ₂₈	10	1.40	8.66	4.63	1.55	0.95	5.45	12.65	8.54	7.04	2.24
C ₂₉	10	1.42	9.15	4.84	1.56	0.95	5.42	12.99	9.08	7.01	2.25
C ₃₀	10	1.44	8.70	4.69	1.56	0.96	5.39	12.72	8.59	6.99	2.26
C ₃₁	10	1.46	9.00	4.83	1.57	0.96	5.36	12.94	8.94	6.97	2.27
C ₃₂	10	1.47	9.36	4.98	1.57	0.97	5.33	13.18	9.34	6.95	2.28
C ₃₃	10	1.49	9.60	5.08	1.57	0.97	5.30	13.34	9.63	6.93	2.29
C ₃₄	10	1.50	9.96	5.20	1.58	0.97	5.28	13.57	10.04	6.91	2.30
C ₃₅	10	1.51	10.23	5.30	1.58	0.97	5.26	13.73	10.35	6.89	2.30
C ₃₆	10	1.53	10.49	5.38	1.58	0.98	5.23	13.89	10.66	6.87	2.31
C ₃₇	10	1.54	10.80	5.47	1.59	0.98	5.21	14.07	11.02	6.86	2.32
C ₃₈	10	1.55	11.07	5.53	1.59	0.98	5.20	14.22	11.34	6.84	2.32
C ₃₉	10	1.56	11.25	5.58	1.59	0.98	5.18	14.32	11.56	6.83	2.33
C ₄₀	10	1.57	11.50	5.63	1.60	0.99	5.16	14.48	11.85	6.82	2.33
Average	340	1.40	6.93	3.49	1.50	0.90	5.93	10.76	7.41	7.41	2.10

^aNPTS is the number of points considered

Table 5. Average error values for heat capacity calculation of hydrocarbons C₇-C₄₀ in the ideal gas state in the temperature range 200-1000 K

	AARE, %	MARE, %	MSE	RMSE	SD	R ²
Huang, 2019	1.40	5.93	157.03	11.41	291.84	1.00
Lee-Kesler, 1976	6.93	10.76	10817.18	85.84	340.56	0.94
Lee-Kesler2, 1976	3.49	7.41	1488.90	32.06	288.00	0.99
Kuznetsov, 2021	1.50	7.41	242.32	14.15	295.85	1.00
Eq. 7	0.90	2.10	180.93	12.17	279.45	1.00

**Fig. 4.** AARE for experimental and computational methods of heat capacity for hydrocarbons from C₇ to C₄₀**Fig. 5.** AARE depending on the carbon number for c_p^{id} of n -alkane

It should be noted that the best results are achieved using the method proposed by Eq. 7, along with Eqs. 3 & 4 [25, 26]. Due to the derivation methodology of Eq. 4, the maximum

calculation error occurs in the low-temperature region, as the formula was initially developed for the temperature range of 300–1500 K. Similarly, Eq. 3 shows its most considerable discrepancies at low temperatures.

It is essential to note that the temperature range of 200–300 K represents typical operating conditions for surface facilities in well production, gathering, and treatment systems at oil, gas, and condensate fields, and should also be considered when developing correlations. Cross-plot comparisons between calculated and experimental data (Fig. 6) clearly demonstrate the limitations of Eqs. 3 & 4 in this low-temperature region.

Significant deviations in the Kesler-Lee correlation are related to the specifics of its derivation, as it was based on experimental data for light and medium paraffin compounds. The proposed Eq. 7 in this study reduces the values of the AARE, MARE, and RMSE parameters compared to the Kesler-Lee correlation, from 6.93%, 10.76%, and 85.84% to 0.90%, 2.10%, and 12.17%, respectively.

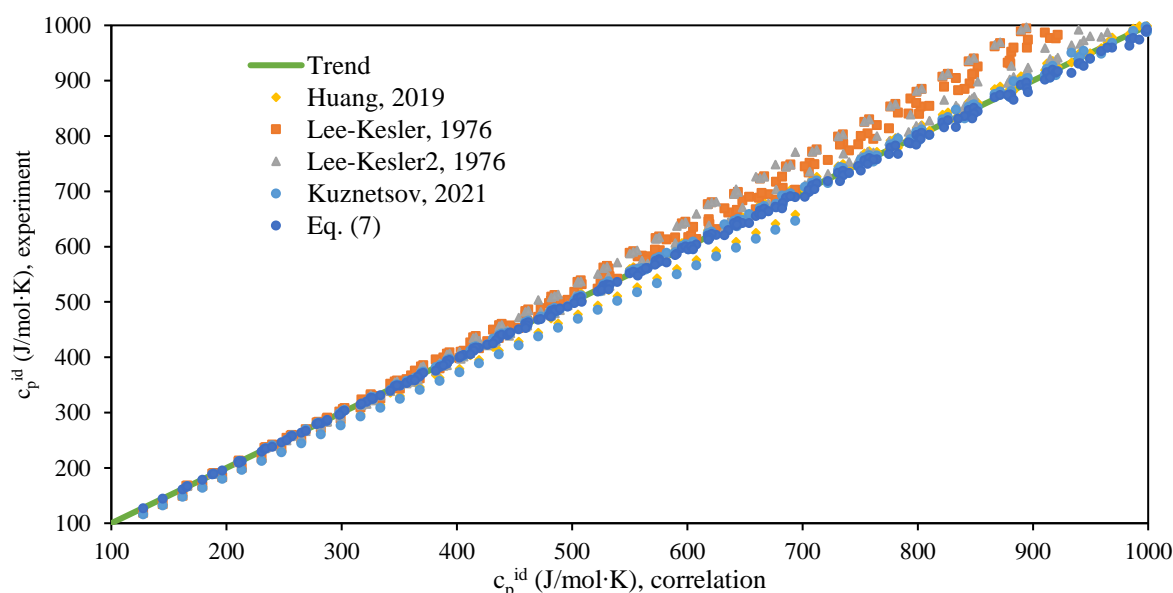


Fig. 6. Cross-plot for different correlations

For independent verification, the presented correlations were tested against the data provided in Table 6.

Table 6. Data for model verification

Formula	Formula	NPTS	Temperature range, K	Ref
C ₇ H ₁₆	n-Heptane	42	182.55-600	[33]
		1	298.15	[34]
C ₈ H ₁₈	n-Octane	52	216.37-730	[33]
C ₉ H ₂₀	n-Nonane	39	219.7-600	[33]
C ₁₀ H ₂₂	n-Decane	44	243.5-675	[33]
C ₁₂ H ₂₆	n-Dodecane	44	263.6-700	[33]

Results of statistical analysis are shown in Table 7.

Table 7. Results of statistical analysis for the isobaric heat capacity of n-alkanes in the ideal gas state

C_n	Huang, 2019	Lee-Kesler, 1976	Lee-Kesler2, 1976	Kuznetsov, 2021	Eq. 7
AARE, %					
C ₇	1.530	1.927	1.337	1.559	0.534
C ₈	1.067	1.182	1.215	0.994	0.530
C ₉	0.571	0.463	0.917	0.609	0.391
C ₁₀	0.512	1.042	0.665	0.541	0.438
C ₁₂	0.474	1.022	0.707	0.533	0.468
MARE, %					
C ₇	13.010	11.564	10.679	14.228	2.501
C ₈	6.082	5.494	5.045	6.862	0.913
C ₉	4.153	4.532	4.129	4.997	0.774
C ₁₀	1.335	2.216	1.138	2.012	0.800
C ₁₂	1.319	2.470	1.248	0.909	0.863
MSE					
C ₇	17.762	18.738	11.743	20.869	1.376
C ₈	11.608	12.199	15.551	9.385	2.358
C ₉	5.145	4.119	17.696	6.295	2.371
C ₁₀	4.419	21.277	9.143	5.369	3.258
C ₁₂	5.268	33.903	15.598	8.607	5.706
RMSE					
C ₇	4.214	4.329	3.427	4.568	1.173
C ₈	3.407	3.493	3.944	3.064	1.535
C ₉	2.268	2.030	4.207	2.509	1.540
C ₁₀	2.102	4.613	3.024	2.317	1.805
C ₁₂	2.295	5.823	3.949	2.934	2.389
SD					
C ₇	52.106	53.542	51.151	52.838	50.178
C ₈	65.920	69.192	65.392	66.638	66.234
C ₉	60.236	61.946	59.176	60.553	59.599
C ₁₀	70.695	74.095	70.012	70.856	71.394
C ₁₂	82.348	86.747	81.715	82.184	83.557
R²					
C ₇	0.993	0.993	0.995	0.992	0.999
C ₈	0.997	0.997	0.996	0.998	0.999
C ₉	0.999	0.999	0.995	0.998	0.999
C ₁₀	0.999	0.996	0.998	0.999	0.999
C ₁₂	0.999	0.995	0.998	0.999	0.999

The obtained results demonstrate that the proposed correlation (Eq. 7) provides the highest accuracy for calculating the isobaric heat capacity of *n*-alkanes in the ideal gas state. To extend the correlation applicability to broader hydrocarbon classes (cycloalkanes and aromatic hydrocarbons), experimental data from [32] for the temperature range 298.15 – 1000 K were considered. The results of the heat capacity discrepancies for various correlations are presented in Tables 8-9.

**Table 8.** Results of the statistical analysis of the isobaric heat capacity of cycloalkanes in the ideal gas state

Name	Huang, 2019	Lee-Kesler, 1976	Lee-Kesler2, 1976	Eq. 7
	AARE, %			
Methylcyclopentane	12.501	3.321	16.057	13.451
Cyclohexane	11.589	6.634	11.940	12.080
Cis-1,3-Dimethylcyclopentane	9.327	2.126	10.662	9.665
Trans-1,3-Dimethylcyclopentane	9.327	2.126	10.662	9.665
Trans-1,2-Dimethylcyclopentane	9.327	2.140	9.123	9.665
Methylcyclohexane	7.465	4.460	9.236	7.342
Ethylcyclopentane	10.595	2.412	8.563	10.937
1,1-Dimethylcyclohexane	7.384	4.903	8.489	7.181
Ethylcyclohexane	6.221	3.917	7.646	6.022
Average	9.304	3.560	10.264	9.557
MARE, %				
Methylcyclopentane	26.952	7.516	25.997	27.411
Cyclohexane	31.150	12.024	19.943	31.624
Cis-1,3-Dimethylcyclopentane	20.922	4.996	18.042	20.907
Trans-1,3-Dimethylcyclopentane	20.922	4.996	18.042	20.907
Trans-1,2-Dimethylcyclopentane	20.922	5.094	14.998	20.907
Methylcyclohexane	20.435	8.953	18.004	20.419
Ethylcyclopentane	23.418	5.495	13.277	23.402
1,1-Dimethylcyclohexane	20.369	9.554	16.469	20.016
Ethylcyclohexane	17.008	7.925	16.025	16.665
Average	22.455	7.395	17.866	22.473
MSE				
Methylcyclopentane	461.216	44.225	1976.847	542.338
Cyclohexane	409.683	398.560	1163.364	432.560
Cis-1,3-Dimethylcyclopentane	375.331	31.069	1274.450	401.791
Trans-1,3-Dimethylcyclopentane	375.331	31.069	1274.450	401.791
Trans-1,2-Dimethylcyclopentane	375.331	30.721	886.155	401.791
Methylcyclohexane	264.379	294.897	1228.578	256.312
Ethylcyclopentane	473.505	47.713	728.796	506.736
1,1-Dimethylcyclohexane	343.651	469.246	1332.976	318.781
Ethylcyclohexane	250.735	313.882	1231.257	231.498
Average	369.907	184.598	1232.986	388.177
RMSE				
Methylcyclopentane	21.476	6.650	44.462	23.288
Cyclohexane	20.241	19.964	34.108	20.798
Cis-1,3-Dimethylcyclopentane	19.373	5.574	35.699	20.045
Trans-1,3-Dimethylcyclopentane	19.373	5.574	35.699	20.045
Trans-1,2-Dimethylcyclopentane	19.373	5.543	29.768	20.045
Methylcyclohexane	16.260	17.173	35.051	16.010
Ethylcyclopentane	21.760	6.907	26.996	22.511
1,1-Dimethylcyclohexane	18.538	21.662	36.510	17.854
Ethylcyclohexane	15.835	17.717	35.089	15.215
Average	19.137	11.863	34.820	19.534
SD				
Methylcyclopentane	69.586	66.992	105.804	72.778
Cyclohexane	68.057	65.966	103.920	71.107
Cis-1,3-Dimethylcyclopentane	79.513	79.240	109.360	81.463
Trans-1,3-Dimethylcyclopentane	79.513	79.240	109.360	81.463
Trans-1,2-Dimethylcyclopentane	79.513	79.280	104.234	81.463
Methylcyclohexane	78.021	78.835	115.566	79.879
Ethylcyclopentane	80.182	78.239	101.877	82.159
1,1-Dimethylcyclohexane	88.927	90.267	130.172	89.807
Ethylcyclohexane	88.879	90.448	126.860	89.759
Average	79.132	78.723	111.906	81.098

Table 9. Results of the statistical analysis of the isobaric heat capacity of aromatic hydrocarbons in the ideal gas state

Name	Huang, 2019	Lee-Kesler, 1976	Lee-Kesler2, 1976	Eq. 7
	AARE, %			
Benzene	44.449	1.838	6.118	46.476
Toluene	36.814	3.656	1.624	37.877
Ethylbenzene	29.540	1.855	1.307	29.952
n-xylene	31.821	4.947	4.687	32.237
m-xylene	31.104	3.887	3.273	31.519
o-xylene	28.935	2.829	1.966	29.353
Styrene	36.963	3.817	1.871	37.492
Cumene	24.927	1.772	1.898	24.879
Average	33.069	3.075	2.843	33.723
MARE, %				
Benzene	58.266	2.956	10.223	59.286
Toluene	46.940	5.049	2.528	47.256
Ethylbenzene	36.815	3.670	2.729	36.677
n-xylene	38.485	6.588	6.107	38.345
m-xylene	37.713	5.680	4.676	37.574
o-xylene	31.833	5.495	5.557	31.700
Styrene	41.160	6.613	3.581	41.075
Cumene	31.093	3.071	3.837	30.643
Average	40.288	4.890	4.905	40.320
MSE				
Benzene	4099.081	11.612	167.629	4657.682
Toluene	4369.442	67.195	8.644	4767.004
Ethylbenzene	4212.719	43.506	22.626	4436.271
n-xylene	4728.561	173.308	151.734	4963.038
m-xylene	4575.847	122.579	82.009	4807.439
o-xylene	4281.519	42.609	16.820	4512.379
Styrene	6055.542	120.660	13.717	6364.818
Cumene	4128.665	41.392	61.789	4186.187
Average	4556.422	77.858	65.621	4836.852
RMSE				
Benzene	64.024	3.408	12.947	68.247
Toluene	66.102	8.197	2.940	69.043
Ethylbenzene	64.905	6.596	4.757	66.605
n-xylene	68.765	13.165	12.318	70.449
m-xylene	67.645	11.072	9.056	69.336
o-xylene	65.433	6.528	4.101	67.174
Styrene	77.817	10.985	3.704	79.780
Cumene	64.255	6.434	7.861	64.701
Average	67.368	8.298	7.210	69.417
SD				
Benzene	90.421	50.541	57.724	95.517
Toluene	99.631	63.925	59.750	103.355
Ethylbenzene	106.924	75.013	73.704	109.315
n-xylene	109.524	76.606	76.028	111.913
m-xylene	108.747	76.011	74.541	111.136
o-xylene	106.940	74.164	71.144	109.331
Styrene	114.134	71.173	65.409	116.702
Cumene	115.210	86.545	87.582	116.330
Average	106.441	71.747	70.735	109.200

Figs. 7-8 shows histograms of the AARE parameter change in heat capacity calculations for cycloalkanes and aromatic hydrocarbons in the ideal gas state.

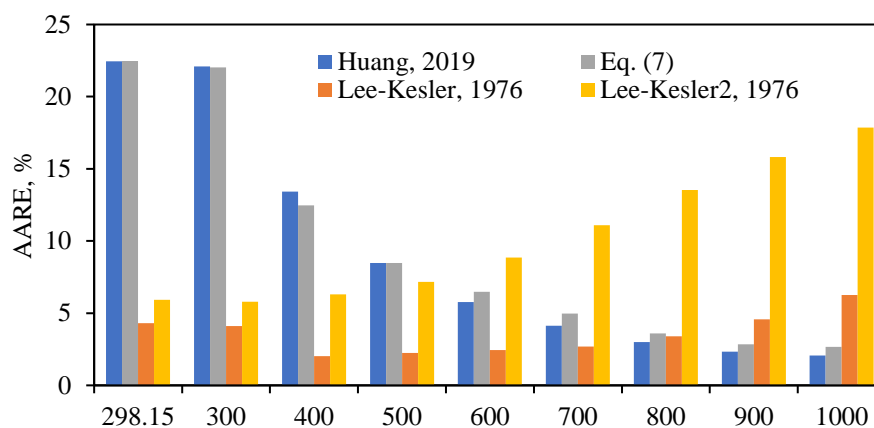


Fig. 7. AARE values for heat capacity calculations of cycloalkanes

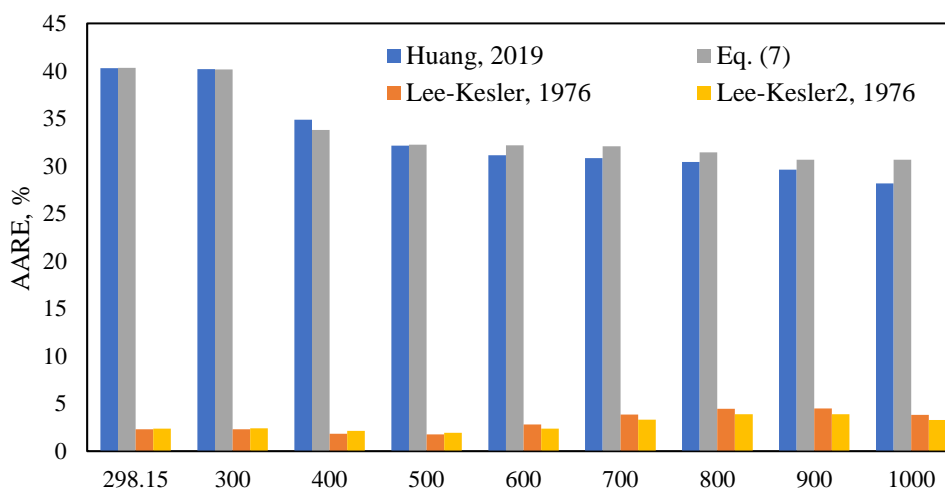


Fig. 8. AARE values for heat capacity calculations of aromatic hydrocarbons

As previously noted, due to the specifics of the Kesler-Lee correlation derivation for light hydrocarbon fractions, Eqs. 7 & 3 are significantly less accurate for such compounds. Fig. 9 shows the dependence of the heat capacity estimation error on molecular weight according to Eq. 7, demonstrating improved accuracy with increasing molecular weight.

Therefore, the proposed correlation (Eq. 7) demonstrates reliable accuracy for n-alkanes within the 200–1000 K temperature range. However, application to pure naphthenic and aromatic compounds requires caution due to significant deviations observed in light fractions. Future incorporation of the specific gravity parameter into Eq. 7 may resolve these discrepancies.

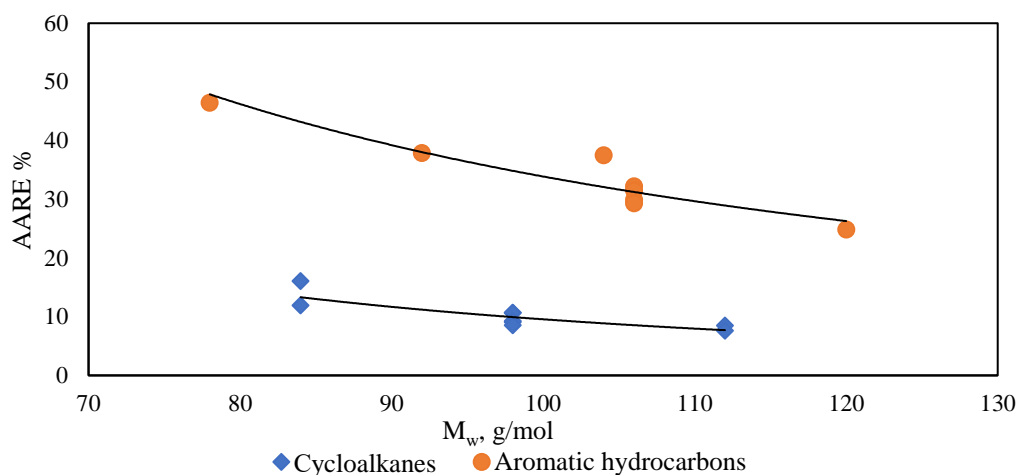


Fig. 9. The dependence of the heat capacity estimation error on molecular weight

According to experimental data (Tables 2 & 3) for hydrocarbons C₇-C₂₀, the Eqs. 10 & 11 allow one to calculate enthalpy and entropy values with AARE not exceeding 0.3% and 0.1%, respectively. The variation of AARE from the carbon number of *n*-alkane is shown in Fig. 10. As enthalpy and entropy depend on heat capacity, the maximum errors are observed at high temperatures close to 1000 K. Similar to heat capacity, the obtained correlation models can be used both for heavier hydrocarbon fractions and for light components down to butane.

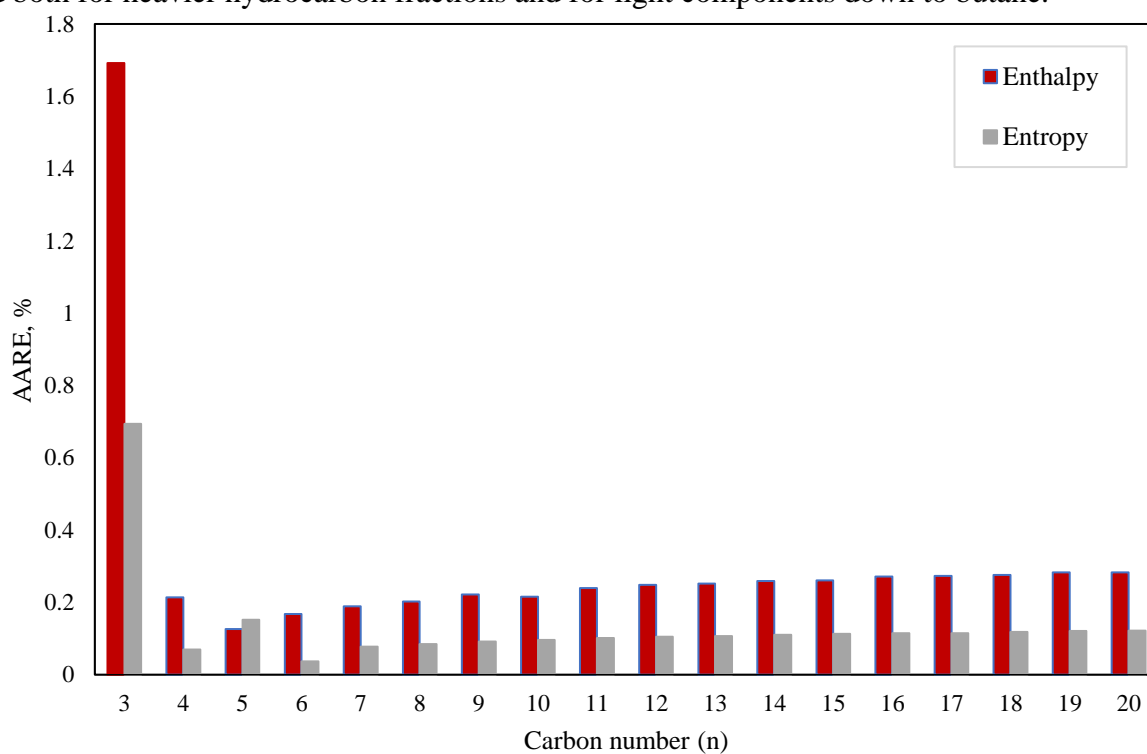


Fig. 10. AARE for enthalpy *H* and entropy *S* of *n*-alkanes

Conclusion

In this study, a new empirical correlation for calculating the thermodynamic properties of hydrocarbons in the ideal gas state has been developed. A comparative analysis with existing methods revealed that the proposed model provides high accuracy, particularly in the low-temperature range (200–300 K), making it suitable for oil, gas, and gas condensate collection and processing systems.

In contrast to traditional methods, the proposed correlation accounts for both temperature dependence and structural characteristics of heavy hydrocarbon fractions, significantly reducing calculation errors compared to the Kesler-Lee model and other correlations for n-alkanes. The model's reliability has been validated through experimental data comparisons and accuracy assessments using statistical metrics. The correlation developed in this work demonstrates a significant reduction in AARE and MARE values compared to the Kesler-Lee correlation from 6.93% and 10.76% to 0.90% and 2.10% respectively. For naphthenic and aromatic compounds, this correlation remains applicable, though with higher uncertainty.

The obtained results can be utilized for more precise thermodynamic modeling in the oil and gas industry, as well as for the development of new hydrocarbon processing and transportation methods. Future research includes adapting the proposed correlation for multicomponent mixtures and integrating it into modern software for PVT analysis.

Nomenclatures

M_w	Molecular weight	[g/mol]
T	Temperature	[K]
T_b	Boiling temperature	[K]
SG	Specific gravity	[-]
c_p^{id}	Heat capacity in the ideal gas state	[J/mol·K]
H_n^{id}	Enthalpy in the ideal gas state	[J/mol]
S_n^{id}	Entropy in the ideal gas state	[J/ mol·K]
K_W	Watson characterization factor	[-]
C_0, C_1, C_2	Coefficients	[-]
A_0, A_1, A_2	Coefficients	[-]
B_0, B_1, B_2	Coefficients	[-]
C_{F0}, C_F	Coefficient	[-]
N	Number of components	
τ	Reduced temperature	

Greek symbols

ω	Acentric factor	[-]
----------	-----------------	-----

Subscripts and indices

N	Carbon number	[-]
P_c	Critical pressure	[bar]
T_c	Critical temperature	[K]
T_{br}	T_b/T_c	

References

- [1] Spencer H.M. Empirical Heat Capacity Equations of Gases and Graphite. *Ind. Eng. Chem.* 1948; 40 (11): 2152–2154. <https://doi.org/10.1021/ie50467a029>
- [2] Passut C.A., Danner R.P.. Correlation of Ideal Gas Enthalpy, Heat Capacity and Entropy, *Ind. Eng. Chem. Process Des. Dev.* 1972; 11(4): 543–546. <https://doi.org/10.1021/i260044a016>

- [3] Aly F.A., Lee L.L. Self-consistent Equations for Calculating the Ideal Gas Heat Capacity, Enthalpy, and Entropy. *Fluid Phase Equil.* 1981; 6: 169–179. [https://doi.org/10.1016/0378-3812\(81\)85002-9](https://doi.org/10.1016/0378-3812(81)85002-9)
- [4] Coniglio L., Rauzy E., Benro C. Representation and Prediction of Thermophysical Properties of Heavy Hydrocarbons. *Fluid Phase Equil.* 1993;87: 53–88. [https://doi.org/10.1016/0378-3812\(93\)85018-H](https://doi.org/10.1016/0378-3812(93)85018-H)
- [5] Benson S.W., Buss J.H. Additivity Rules for the Estimation of Molecular Properties. Thermodynamic Properties. *J. Chem. Phys.* 1958;29: 546–572. <https://doi.org/10.1063/1.1744539>
- [6] Bures M., Maier V., Zabransky M. Modification of Benson Method for Estimation of Ideal-Gas Heat Capacities. *Chem. Eng. Sci.* 1981;36: 529–537. [https://doi.org/10.1016/0009-2509\(81\)80142-x](https://doi.org/10.1016/0009-2509(81)80142-x)
- [7] Joback K.G., Reid R.C. Estimation of Pure-Component Properties from Group-Contributions. *Chemical Engineering Communications.* 1987;57: 233–243. <https://doi.org/10.1080/00986448708960487>
- [8] Constantinou L., Gani R. New Group Contribution Method for Estimating Properties of Pure Compounds. *AICHE Journal.* 1994; 40: 1697–1710. <https://doi.org/10.1002/aic.690401011>
- [9] Watson K.M., Nelson E.F. Improved methods for approximating critical and thermal properties of petroleum fractions, *Ind. Eng. Chem.* 1933, 25 (8): 880-887. <https://doi.org/10.1021/ie50284a012>
- [10] Daubert T.E., Danner R.P. Eds, API Technical Data Book-Petroleum Refining, 6th ed., American Petroleum Institute (API), Washington, DC, 1997.
- [11] Cavett R.H. Physical Data for Distillation Calculations, Vapor-Liquid Equilibria. *Proceedings of 27th API Meeting, API Division of Refining.* 1962; 42(3): 351–366.
- [12] Kesler M.G., Lee B.I., Improve Prediction of Enthalpy of Fractions, *Hydrocarbon Processing* 55 (1976) 153–158.
- [13] Lee B.I., Kesler M.G. A Generalized Thermodynamic Correlation Based on Three-Parameter Corresponding States, *AICHE Journal* 21(3) (1975) 510–527. <https://doi.org/10.1002/aic.690210313>
- [14] Riazi M.R., Daubert T.E. Simplify Property Predictions. *Hydrocarbon Processing.* 1980; 59 (3): 115–116.
- [15] Riazi M.R., Daubert T.E. Characterization Parameters for Petroleum Fractions. *Industrial and Engineering Chemistry Research.* 1987; 26: 755–759. <https://doi.org/10.1021/ie00064a023>
- [16] Riazi M.R., Al-Sahhaf T. Physical Properties of n-Alkanes and n-Alkyl Hydrocarbons: Application to Petroleum Mixtures. *Industrial and Engineering Chemistry Research.* 1995;34 (11): 4145–4148. <https://doi.org/10.1021/ie00038a062>
- [17] Twu C.H. An Internally Consistent Correlation for Predicting the Critical Properties and Molecular Weights of Petroleum and Coal-Tar Liquids. *Fluid Phase Equilibria.* 1984;16: 137–150. [https://doi.org/10.1016/0378-3812\(84\)85027-X](https://doi.org/10.1016/0378-3812(84)85027-X)
- [18] Pedersen K.S., Milter J., Sorensen H. Cubic Equations of State Applied to HT/HP and Highly Aromatic Fluids. *SPE Journal.* 2002;9: SPE 77385. <https://doi.org/10.2118/77385-MS>
- [19] Pedersen K.S., Thomassen P., Fredenslund A. Characterization of Gas Condensate Mixtures, presented in C7+ Fraction Characterization (Chorn, L.G. Mansoori, G.A.). *Taylor & Francis.* New York; 1989.
- [20] Pedersen K.S., Blilie A.L., Meisingset K.K. PVT Calculations on Petroleum Reservoir Fluids Using Measured and Estimated Compositional Data for the Plus Fraction. *I&EC Research.* 1992; 31 (5): 1378-1384. <https://doi.org/10.1021/ie00005a019>
- [21] Pedersen K.S., Christensen P.L., Phase Behavior of Petroleum Reservoir Fluids. *Taylor & Francis Group, USA: Boca Raton;* 2007. 406 p. <https://doi.org/10.1201/b17887>
- [22] Korsten H., Characterization of Hydrocarbon Systems by DBE Concept. *AICHE Journal.* 1997; 43 (6): 1559–1568. <https://doi.org/10.1002/aic.690430619>
- [23] Riazi M.R., Characterization and Properties of Petroleum Fractions, ASTM International. 2005, 425 p. <https://doi.org/10.1520/MNL50-EB>



- [24] Lastovka V., Shaw J.M. Predictive Correlations for Ideal Gas Heat Capacities of Pure Hydrocarbons and Petroleum Fractions. *Fluid Phase Equil.* 2013; 356: 338–370. <https://doi.org/10.1016/j.fluid.2013.07.023>
- [25] Huang D., Yang D. Improved Enthalpy Prediction of Hydrocarbon Fractions with a Modified Alpha Function for the Peng-Robinson Equation of State. *Fuel.* 2019;255: 115840. <https://doi.org/10.1016/j.fuel.2019.115840>
- [26] Kuznetsov N.M., Frolov S.M. Heat Capacities and Enthalpies of Normal Alkanes in an Ideal Gas State. *Energies.* 2021;14: 2641. <https://doi.org/10.3390/en14092641>
- [27] Kuznetsov N.M., Frolov S.M. Heat Capacity and Enthalpy of Saturated Hydrocarbons (Alkanes) in the Ideal Gas State. *Combustion and Explosion.* 2020; 13 (2): 113–117. (in Russian)
- [28] Coniglio L., Daridon J.L. A Group Contribution Method for Estimating Ideal Gas Heat Capacities of Hydrocarbons. *Fluid Phase Equilibria.* 1997;139: 15–35. [https://doi.org/10.1016/S0378-3812\(97\)00143-X](https://doi.org/10.1016/S0378-3812(97)00143-X)
- [29] Yushchenko T.S., Sannikova I.A., Kulkov M.G., Brusilovsky A.I., Salakhidinova G.T., Aliev A.E., Gavrilov A.E. Identification of the Composition and Assessment of the Influence of the Solid Hydrocarbon Phase in the Reservoir on the Behavior of the Mobile Fluid of the Bazhenov Formation During the Reservoir Development. *Georesursy.* 2024; 26 (1): 78–99. <https://doi.org/10.18599/grs.2024.1.7>
- [30] Katz D.L., Firoozabadi A. Predicting Phase Behavior of Condensate/Crude Oil Systems Using Methane Interaction Coefficients. *Journal of Petroleum Technology.* 1978; 30: 1649–1655. <https://doi.org/10.2118/6721-PA>
- [31] Vargaftik N.B. Handbook of Thermophysical Properties of Gases and Liquids, Moscow: Nauka; 1972; 721 p. (in Russian)
- [32] Malyshev V.L., Nurgalieva Ya.F., Moiseeva E.F. Comparative Study of Empirical Correlations and Equations of State Effectiveness for Compressibility Factor of Natural Gas Determination. *PeriodicoTcheQuimica.* 2021; 18(38): 188–213. [10.52571/PTQ.v18.n38.2021.14_MALYSHEV_pgs_188_213.pdf](https://doi.org/10.52571/PTQ.v18.n38.2021.14_MALYSHEV_pgs_188_213.pdf)
- [33] NIST Chemistry WebBook, <https://webbook.nist.gov/chemistry/fluid>
- [34] Colgate S.O., Sona C.F., Reed K.R., Sivaraman A. Experimental ideal gas reference state heat capacities of gases and vapors *Journal of Chemical and Engineering Data.* 1990; 35 (1), 1–5. <https://pubs.acs.org/doi/10.1021/jc00059a001>

How to cite: Malyshev V.L., Moiseeva E.F. New Correlations for Predicting Thermodynamic Properties of Hydrocarbons in the Ideal Gas State. *Journal of Chemical and Petroleum Engineering* 2025; 59(2): 405-426.